#### **Tailor-made Carbon Molecular Sieve Membranes** (CMSMs) for gas separation in membrane reactors

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### Outlook

- Introduction
- CMSMs
- Applications of CMSMs
- Q&A



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# Introduction

#### **Energy resources**

- The change in 30 years
- Dominated by fossil fuels (61%)
- Increased electricity production



https://www.iea.org/data-and-statistics/data-product/world-energy-balances-highlights







### Introduction

#### SEPARATION OF CHEMICALS

- 50% of US industrial energy use
- 10-15% of total energy consumption
- New technologies are required









### Introduction

#### MEMBRANE SEPARATION TECHNOLOGY

- Carbon Molecular Sieve Membranes (CMSMs)
- Separation based on molecular size and/or affinity
- Sub-nanometer range





### CMSMs

- Made via pyrolysis of a <u>thermosetting</u> polymer
  - Resorcinol- formaldehyde resin
  - Novolac
  - Polyimide based ...
- <u>Porous</u> structure
- Modification of pore size and pore size distribution







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### CMSMs

How is it made?

- 1. Precursor synthesis
- 2. Dipping solution preparation
- 3. Coating
- 4. Polymerization
- 5. Carbonization
- 6. Post treatment

Surface diffusion and molecular sieving are the common transport mechanisms











### CMSMs

#### What could be separated?

Any desired molecule with different kinetic diameter compared to other molecules and/or difference in polarity (hydrophilicity/hydrophobicity)

#### Processes which have:

- Operational temperatures up to 700 °C (no oxygen)
- Operational pressures up to 200 Bar
- Configurations of
  - a. Gas separation
  - b. Pervaporation (liquid/vapor)
  - c. Vapor permeation
  - d. Selective gas distribution













H<sub>2</sub> separation

Al(acac)<sub>3</sub> effect on pore size distribution (PSD)



Narrow pore size distribution (PSD)







Inorganic Membranes & Membrane Reactors



https://doi.org/10.1016/j.ijhydene.2022.02.198

#### H<sub>2</sub> separation

#### Al(acac)<sub>3</sub> effect on pore size distribution (PSD)

- > 382  $H_2/N_2$  ideal selectivity
- Stable performance up to 350 °C





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Effect of degree of polymerization on PSD Resorcinol-formaldehyde resin



https://doi.org/10.3390/membranes12090847









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Humidifier

Drain

**R80** 

0.3 0.4 0.5

0.2-10 nl/min

7 bar

N<sub>2</sub>

DI water

Ð

Ta

R100

Membrane Reactor

R60

0.6 0.7 0.8

Pore width (nm)



1.2

(TC)

Oven

R30

TC

\_\_\_\_\_

Cooler

**∀** Drain

Condensate

1.0

0.9

1.1

PE

Air extraction

Film flow meter



#### Fine tuning the PSD with degree of polymerization and oxygen post treatment

https://doi.org/10.3390/membranes12090847



areNH<sub>3</sub>a



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-ER

CO<sub>2</sub> separation CO<sub>2</sub>/CH<sub>4</sub> (Biogas upgrading)



areNH<sub>3</sub>a



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CO<sub>2</sub> separation CO<sub>2</sub>/CH<sub>4</sub> (Biogas upgrading)













#### CO<sub>2</sub> separation CO<sub>2</sub>/CH<sub>4</sub> (Natural gas purification)

Increased  $CO_2/CH_4$  ideal selectivity with increasing ethylenediamine content

- Increasing the ideal selectivity dependance on the operational pressure with increasing the ethylenediamine content in the dipping solution because of increased surface diffusion and adsorption sites
- Stable performance at 40 bar operational pressure

#### Effect of pressure on the CMSMs permselectivity



![](_page_14_Picture_7.jpeg)

![](_page_14_Picture_8.jpeg)

![](_page_14_Picture_9.jpeg)

#### CO<sub>2</sub> separation CO<sub>2</sub>/CH<sub>4</sub> (Natural gas purification)

Novolac – Ethylenediamine co-polymerization

Ethylenediamine effect:

- Reduction in surface roughness (Ra and Rz)
- Increase of membrane stability at higher temperatures and uniform permeance (less thickness variation)

	Surface roughness (3D laser microscopy)			
Membrane	50x	(nm)	150 x	(nm)
Welliorane	Ra*	Rz**	Ra	Rz
E 0	286	2021	202	1280
E 0.4	227	1429	69	475
E 1.2	100	734	94	652

\* the average surface roughness, \*\* difference between the tallest (peak) and deepest (valley) on the surface.

https://doi.org/10.1016/j.jcou.2022.102378

![](_page_15_Picture_9.jpeg)

![](_page_15_Picture_10.jpeg)

![](_page_15_Picture_11.jpeg)

#### 3D laser confocal microscopy

![](_page_15_Figure_13.jpeg)

![](_page_15_Figure_14.jpeg)

![](_page_15_Picture_15.jpeg)

CO<sub>2</sub> separation at elevated pressures and temperatures CO<sub>2</sub>/Mix (Steel mill off gas)

- 152 CO<sub>2</sub>/N<sub>2</sub> real selectivity at 300 °C
- 92 % CO<sub>2</sub> in the permeate
- Stable performance

![](_page_16_Figure_5.jpeg)

#### He separation from natural gas

- Shifting the smaller average pore size with increasing the polymerization temperature but there is an optimum
- CMSM carbonized at 850 °C and polymerized at 140 °C , contains 89% of the pores below 0.3 nm in diameter

![](_page_17_Picture_4.jpeg)

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![](_page_17_Figure_5.jpeg)

![](_page_17_Picture_6.jpeg)

![](_page_17_Picture_7.jpeg)

![](_page_17_Picture_8.jpeg)

#### **Bioethanol dehydration via pervaporation (2021)**

Effect of support roughness, coating parameters investigated The higher oligomer's molecular weight resulted in higher water/ethanol selectivities.

![](_page_18_Figure_3.jpeg)

#### Thanks for your time and attention Questions, suggestions are welcome

![](_page_19_Picture_1.jpeg)

![](_page_19_Picture_2.jpeg)

![](_page_19_Picture_3.jpeg)

![](_page_19_Picture_5.jpeg)